

## NUMERICAL STUDY OF MAGNETO-HYDRODYNAMIC THREE-DIMENSIONAL COUETTE FLOW THROUGH A MEDIUM IN THE PRESENCE OF HEAT SOURCE

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### 1 Abstract

In the present article numerical simulation is made using an implicit finite difference scheme on Couette flow of a viscous incompressible electrically conducting fluid between two horizontal parallel porous flat plates in the presence of heat source. A magnetic field is applied normal to the fluid flow. The plate in uniform motion and stationary plate are subjected to constant suction and the transverse sinusoidal injection of the fluid respectively. This type of sinusoidal injection velocity makes the flow three-dimensional. Obtaining exact solution of this problem is very difficult, so the governing non-linear equations with boundary conditions are transformed to ordinary and partial differential equations of zeroth and first order respectively, using perturbation method. Exact solutions corresponding to the zeroth order differential equations are obtained in the case of  $\varepsilon = 0$ . The first order differential equations in the case of  $\varepsilon \neq 0$  are reduced to ordinary differential equations using appropriate substitutions. Then, these resultant equations are transformed to system of equations using implicit-finite difference method, for which simulation is carried out by coding in C-Program. The results obtained for Nusselt number are discussed graphically and compared with previously published work in the absence of heat source parameter. These comparisons have shown a good agreement between the results. From this study, it is observed that the temperature and Nusselt number increase in the presence of heat source parameter.

### Key words

Three-dimensional, Couette flow, magnetic field, heat source, permeability, Finite-difference method;

### Introduction

In recent years the fluid flow through porous media have attracted the attention of a number of researchers because of their applications in many branches of science and technology. In fact a porous material containing the fluid is a non-homogeneous medium. For the sake of analysis it is also considered as a homogeneous medium, by considering its dynamical properties to be equal to the local averages of the original non-homogeneous continuum. So a difficult problem of the fluid flow through a porous medium gets reduced to the flow problem of a homogeneous fluid with additional resistance. A series of investigation have been made by different scholars where the porous medium is either bounded by horizontal or vertical surfaces. Unsteady flow of a conducting fluid through porous medium in the presence of magnetic field was studied by Gulub Ram and Mishra

[1]. Oscillatory flow through porous medium bounded by a horizontal porous plate with variable suction velocity was analysed by Varshney [2]. Unsteady free-convection flow through a porous medium bounded by an infinite porous plate with variable temperature and constant suction was investigated by Raptis [3]. Further, Raptis and Perdakis [4] discussed the oscillatory free convective flow through a porous medium bounded by a vertical porous plate with constant suction when the velocity of free stream oscillates about a mean in time. Gersten and Gross [6] studied the three dimensional convection flow and heat transfer through a porous medium, later this study was extended by Singh *et al* [5] by considering effect periodic suction velocity into account. The variation of such suction velocity on different heat transfer flow problems along flat and vertical porous plates have also been studied by Singh [7, 8].

The study of channel flows through porous medium play a vital role in many scientific and engineering investigations like geophysical applications, for example, In chemical engineering for filtration and purification processes; to study the underground water resources in agriculture engineering; to study the movement of natural gas, oil and water through the oil channels/reservoirs in petroleum technologies. Due to these applications, Couette flow with transpiration cooling for ordinary medium has been studied by Singh [9]. Singh and Sharma [10] later investigated magneto hydrodynamic three-dimensional Couette flow with transpiration cooling. Recently Singh *et al* [11] analysed the effect of permeability of the porous medium on three-dimensional Couette flow and heat transfer. Three-dimensional Couette flow and heat transfer through a porous medium with variable permeability was discussed by Choudhary and Sharma [12]. Singh [13] studied the influence of a moving magnetic field on three-dimensional Couette flow. The effect of magneto hydrodynamics on three-dimensional viscous incompressible heat transfer flow between two horizontal parallel porous plates with periodic injection/suction was discussed by Pawan Kumar Sharma and Chaudhary [14]. Sharma and Yadav [15] analyzed the effects of heat transfer on three dimensional flow between a stationary porous plate and a moving porous plate. Three Couette flow between two parallel plates with transpiration cooling through a porous medium in the slip flow regime has been investigated by Jain *et al.* [16]. Govindarajan *et al.* [17] discussed the three-dimensional Couette flow of a viscous incompressible dusty fluid with transpiration cooling.

Das *et al.* [18] analyzed the three dimensional Couette flow and heat transfer in the presence of a transverse magnetic field. The effect of viscous dissipation on Couette flow of a viscous incompressible fluid through a porous medium between two infinite horizontal parallel porous flat plates in the presence of transverse magnetic field is studied by Srihari *et al* [19]. Das *et al.* [20] studied the effects of constant suction and sinusoidal injection on hydromagnetic three dimensional Couette flow of a viscous incompressible fluid between two infinite horizontal parallel porous flat plates. An analytical solution for three-dimensional mixed convective mass transfer flow along an infinite vertical porous plate by the presence of a magnetic field was obtained Ahmed [21]. Ahmed and Talukdar [22] discussed the effect of chemical reaction in the presence of heat sink on oscillatory three-dimensional flow with mass transfer past a vertical plate with thermal diffusion. Recently, the effects of an exponential injection/suction parameter on three-dimensional

Couette flow of a dusty fluid with heat transfer was analysed by Gireesha [23]. Hayat et al. [24] investigated the three-dimensional flow of viscous fluid with convective boundary conditions and heat generation/absorption. Due to the practical applications of Magneto hydrodynamics in the field of power generation, geophysics and astrophysics, Shehzad et al [26] studied the effect of magnetic field on three-dimensional flow of an Oldroyd-B nanofluid over a radiative surface. Baag and Mishra [25] made an analysis of heat and mass transfer on three-dimensional hydromagnetic nano-fluid flow.

The effect of heat source has not been considered in most of the previous investigations but it plays an important role in maintaining heat transfer at desired level in the fields of Nuclear power plants, gas turbines and the various propulsion devices for aircraft, missiles, satellites and space vehicles. So, in the present paper an attempt has been made to study the effect of heat source on Couette flow of a viscous incompressible fluid through a porous medium between two horizontal parallel porous flat plates. A magnetic field is introduced perpendicular to the flow. In order to describe the physics of the problem, first the non-linear boundary value problem is transformed to ordinary and partial differential equations of zeroth and first order respectively, using perturbation method. Obtaining exact solution for first order partial differential equations with boundary conditions is very difficult so, using appropriate substitutions; these equations are reduced to coupled non-linear ordinary differential equations, then they are solved numerically using finite difference method.

## 2 Mathematical analysis

Couette flow of an incompressible viscous electrically conducting fluid between two parallel porous flat plates is considered. A co-ordinate system is introduced with the origin at the lower stationary plate, lying horizontally on  $x^* - z^*$  plane. The upper plate, which is in uniform motion  $U$ , is separated by a distance 'd' from the lower plate. The  $y^*$  - axis is taken perpendicular to the planes of the plates. A magnetic field is applied normal to the fluid flow. The lower and the upper plates are assumed to be at constant temperatures  $T_0$  and  $T_1$ , respectively, with  $T_1 > T_0$ . The upper plate is subjected to a constant suction  $V$  whereas the lower plate to a transverse sinusoidal injection velocity distribution of the form:

$$v^*(z^*) = V(1 + \varepsilon \cos \pi z^* / d). \quad (1)$$

where  $\varepsilon (\ll 1)$  is a positive constant. Without loss of generality, the distance 'd' is considered as wavelength of the injection velocity. The velocity components  $u^*$ ,  $v^*$  and  $w^*$  are considered in the directions of  $x^*$ ,  $y^*$  and  $z^*$ , respectively. The governing equations are derived with the assumption that the flow is steady and laminar, and is of a finitely conducting fluid. For this fully developed laminar flow problem, all physical quantities are independent of  $x^*$  but the flow remains three-dimensional due to the periodic injection velocity (1). Thus, under these assumptions, the problem is governed by the following equations:

$$\frac{\partial v^*}{\partial y^*} + \frac{\partial w^*}{\partial z^*} = 0 \tag{2}$$

$$v^* \frac{\partial u^*}{\partial y^*} + w^* \frac{\partial u^*}{\partial z^*} = \nu \left( \frac{\partial^2 u^*}{\partial y^{*2}} + \frac{\partial^2 u^*}{\partial z^{*2}} \right) - \frac{\nu u^*}{K^*} - \frac{\sigma B_0^2}{\rho} u^* \tag{3}$$

$$v^* \frac{\partial v^*}{\partial y^*} + w^* \frac{\partial v^*}{\partial z^*} = -\frac{1}{\rho} \frac{\partial p^*}{\partial y^*} + \nu \left( \frac{\partial^2 v^*}{\partial y^{*2}} + \frac{\partial^2 v^*}{\partial z^{*2}} \right) - \frac{\nu}{K^*} v^* \tag{4}$$

$$v^* \frac{\partial w^*}{\partial y^*} + w^* \frac{\partial w^*}{\partial z^*} = -\frac{1}{\rho} \frac{\partial p^*}{\partial z^*} + \nu \left( \frac{\partial^2 w^*}{\partial y^{*2}} + \frac{\partial^2 w^*}{\partial z^{*2}} \right) - \frac{\nu}{K^*} w^* - \frac{\sigma B_0^2}{\rho} w^* \tag{5}$$

$$\rho C_p \left( v^* \frac{\partial T^*}{\partial y^*} + w^* \frac{\partial T^*}{\partial z^*} \right) = k \left( \frac{\partial^2 T^*}{\partial y^{*2}} + \frac{\partial^2 T^*}{\partial z^{*2}} \right) + Q(T^* - T_0) \tag{6}$$

**The boundary conditions of the problem are:**

$$\left. \begin{aligned} y^* = 0: u^* = 0, v^*(z^*) = V(1 + \varepsilon \cos \pi z^*/d), w^* = 0, T^* = T_0^* \\ y^* = d: u^* = U, v^* = V, w^* = 0, T^* = T_1 \end{aligned} \right\} \tag{7}$$

Substitution the following non dimensional quantities:

$$\begin{aligned} y = \frac{y^*}{d}, z = \frac{z^*}{d}, u = \frac{u^*}{U}, v = \frac{v^*}{U}, \\ w = \frac{w^*}{U}, p = \frac{p^*}{\rho U^2}, \theta = \frac{T^* - T_0}{T_1 - T_0} \end{aligned} \tag{8}$$

into equations (2) to (7), implies the following

$$\frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} = 0 \tag{9}$$

$$v \frac{\partial u}{\partial y} + w \frac{\partial u}{\partial z} = \frac{1}{\text{Re}} \left( \frac{\partial^2 u}{\partial y^2} + \frac{\partial^2 u}{\partial z^2} \right) - \frac{u}{\text{Re} K} - \frac{M^2}{\text{Re}} u \tag{10}$$

$$v \frac{\partial v}{\partial y} + w \frac{\partial v}{\partial z} = -\frac{\partial p}{\partial y} + \frac{1}{\text{Re}} \left( \frac{\partial^2 v}{\partial y^2} + \frac{\partial^2 v}{\partial z^2} \right) - \frac{v}{\text{Re} K} \tag{11}$$

$$v \frac{\partial w}{\partial y} + w \frac{\partial w}{\partial z} = -\frac{\partial p}{\partial z} + \frac{1}{\text{Re}} \left( \frac{\partial^2 w}{\partial y^2} + \frac{\partial^2 w}{\partial z^2} \right) - \frac{w}{\text{Re} K} - \frac{M^2}{\text{Re}} w \tag{12}$$

$$v \frac{\partial \theta}{\partial y} + w \frac{\partial \theta}{\partial z} = \frac{1}{\text{Re Pr}} \left( \frac{\partial^2 \theta}{\partial y^2} + \frac{\partial^2 \theta}{\partial z^2} \right) + \frac{S}{\text{Re Pr}} \theta \tag{13}$$

with boundary conditions in non-dimensional form

$$\left. \begin{aligned} y = 0: u = 0, v(z) = \alpha(1 + \varepsilon \cos \pi z), w = 0, \theta = 0 \\ y = 1: u = 1, v = \alpha, w = 0, \theta = 1 \end{aligned} \right\} \tag{14}$$

where,

$$S = \frac{Qd^2}{k} \text{ (Heat source parameter), } Re = \frac{Ud}{\nu} \text{ (Injection/suction parameter),}$$

$$Pr = \frac{\mu C_p}{k} \text{ (Prandtl number), } K = \frac{K^*}{d^2} \text{ (Permeability parameter),}$$

$$M = B_0 d \sqrt{\frac{\sigma}{\mu}} \text{ (Magnetic parameter),}$$

### 3. Method of solution

In order to solve these non-linear differential equations, the solutions of the following form are assumed because the amplitude  $\varepsilon$ , ( $\ll 1$ ) of the injection velocity is very small:

$$f(y, z) = f_0(y) + \varepsilon f_1(y, z) + \varepsilon^2 f_2(y, z) + \dots \quad (15)$$

where  $f$  stands for  $u, v, w, p$  and  $\theta$ .

Substituting the equation (15) into equations(9) to (13) and equating the like power of  $\varepsilon$ , we get the following zeroth and first order equations for the case of  $\varepsilon = 0$ , and  $\varepsilon \neq 0$ , respectively.

#### 3.1 Zeroth order equations for the case $\varepsilon=0$

$$\frac{dv_0}{dy} = 0 \quad (16)$$

$$\frac{d^2 u_0}{dy^2} - \alpha Re \frac{du_0}{dy} - \left( M^2 + \frac{1}{K} \right) u_0 = 0 \quad (17)$$

$$\frac{d^2 \theta_0}{dy^2} - \alpha Re Pr \frac{d\theta_0}{dy} + S \theta_0 = 0 \quad (18)$$

The corresponding boundary conditions reduces to

$$y = 0; u_0 = 0, v_0 = \alpha, w_0 = 0, \theta_0 = 0 \quad (19)$$

$$y = 1; u_0 = 1, v_0 = \alpha, w_0 = 0, \theta_0 = 1$$

The solutions of the above equations are given by

$$u_0(y) = \frac{e^{m_1 y} - e^{m_2 y}}{e^{m_1} - e^{m_2}}, \quad (20)$$

$$\theta_0(y) = \frac{e^{a_2 y} - e^{a_1 y}}{e^{a_2} - e^{a_1}} \quad (21)$$

$$v_0 = \alpha = 1, w_0 = 0, p_0 = \text{constant} \quad (22)$$

where

$$m_1 = \frac{1}{2} \left[ Re + \sqrt{Re^2 + 4 \left( M^2 + \frac{1}{K} \right)} \right], \quad m_2 = \frac{1}{2} \left[ Re - \sqrt{Re^2 + 4 \left( M^2 + \frac{1}{K} \right)} \right]$$

$$a_1 = \frac{1}{2} \left[ \text{Re Pr} + \sqrt{(\text{Re Pr})^2 - 4S} \right] \quad a_2 = \frac{1}{2} \left[ \text{Re Pr} - \sqrt{(\text{Re Pr})^2 - 4S} \right]$$

### 3.2 First order equations for the case $\varepsilon \neq 0$

$$\frac{\partial v_1}{\partial y} + \frac{\partial w_1}{\partial z} = 0 \tag{23}$$

$$v_1 \frac{\partial u_0}{\partial y} + \frac{\partial u_1}{\partial y} = \frac{1}{\text{Re}} \left( \frac{\partial^2 u_1}{\partial y^2} + \frac{\partial^2 u_1}{\partial z^2} \right) - \frac{u_1}{\text{Re} K} - \frac{M^2}{\text{Re}} u_1 \tag{24}$$

$$\frac{\partial v_1}{\partial y} = -\frac{\partial p_1}{\partial y} + \frac{1}{\text{Re}} \left( \frac{\partial^2 v_1}{\partial y^2} + \frac{\partial^2 v_1}{\partial z^2} \right) - \frac{v_1}{\text{Re} K} \tag{25}$$

$$\frac{\partial w_1}{\partial y} = -\frac{\partial p_1}{\partial z} + \frac{1}{\text{Re}} \left( \frac{\partial^2 w_1}{\partial y^2} + \frac{\partial^2 w_1}{\partial z^2} \right) - \frac{w_1}{\text{Re} K} - \frac{M^2}{\text{Re}} w_1 \tag{26}$$

$$v_1 \frac{\partial \theta_0}{\partial y} - \frac{\partial \theta_1}{\partial y} = \frac{1}{\text{Re Pr}} \left( \frac{\partial^2 \theta_1}{\partial y^2} + \frac{\partial^2 \theta_1}{\partial z^2} \right) + \frac{S}{\text{Re Pr}} \theta_1 \tag{27}$$

The corresponding boundary conditions reduced to the following form:

$$\begin{aligned} y = 0; u_1 = 0, v_1 = \cos \pi z, w_1 = 0, \theta_1 = 0 \\ y = 1; u_1 = 0, v_1 = 0, w_1 = 0, \theta_1 = 0 \end{aligned} \tag{28}$$

The equations, which are obtained for the case,  $\varepsilon \neq 0$  describe the three-dimensional flow through porous medium.

In order to solve the equations (23), (25) and (26), we assume  $v_1$ ,  $w_1$  and  $p_1$  as follows:

$$v_1(y, z) = v_{11}(y) \cos \pi z \tag{29}$$

$$w_1(y, z) = -\frac{1}{\pi} \frac{dv_{11}(y)}{dy} \sin \pi z \tag{30}$$

$$p_1(y, z) = p_{11}(y) \cos \pi z \tag{31}$$

In the above equations (29) and (30) are chosen so that the equation of continuity (23) is satisfied. Substitution of the equations (29), (30) and (31) into (25) and (26), gives the following

$$\frac{d^2 v_{11}}{dy^2} - \text{Re} \frac{dv_{11}}{dy} - \left( \pi^2 + \frac{1}{K} \right) v_{11} = \text{Re} \frac{dp_{11}}{dy} \tag{32}$$

$$\frac{d^3 v_{11}}{dy^3} - \text{Re} \frac{d^2 v_{11}}{dy^2} - \left( \pi^2 + M^2 + \frac{1}{K} \right) \frac{dv_{11}}{dy} = \text{Re} \pi^2 p_{11} \tag{33}$$

Elimination of the terms  $\frac{dp_{11}}{dy}$  and  $p_{11}$  in the equations (32) and (33), implies

$$\frac{d^4 v_{11}}{dy^4} - \text{Re} \frac{d^3 v_{11}}{dy^3} - \left( M^2 + \frac{1}{K} + 2\pi^2 \right) \frac{d^2 v_{11}}{dy^2} + \text{Re} \pi^2 \frac{dv_{11}}{dy} + \left( \pi^4 + \frac{\pi^2}{K} \right) v_{11} = 0 \quad (34)$$

The corresponding boundary conditions given by

$$\begin{aligned} y = 0: v_{11} &= 0, \\ y = 1: v_{11} &= 0, \end{aligned} \quad (35)$$

In order to obtain the solution for main flow velocity ( $u_1$ ) and temperature ( $\theta_1$ ), the following are assumed

$$u_1(y, z) = u_{11}(y) \cos \pi z \quad (36)$$

$$\theta_1(y, z) = \theta_{11}(y) \cos \pi z \quad (37)$$

Substituting (36) and (37) in to the partial differential equations (24) and (27) and in their corresponding boundary conditions, we get the following

$$\frac{d^2 u_{11}}{dy^2} - \text{Re} \frac{du_{11}}{dy} - \left( M^2 + \frac{1}{K} + \pi^2 \right) u_{11} = \text{Re} v_{11} \frac{du_0}{dy} \quad (38)$$

$$\frac{d^2 \theta_{11}}{dy^2} - \text{Re Pr} \frac{d\theta_{11}}{dy} - (\pi^2 - S) \theta_{11} = \text{Re Pr} v_{11} \frac{d\theta_0}{dy} \quad (39)$$

with boundary conditions

$$\begin{aligned} y = 0: u_{11} &= 0, \theta_{11} = 0 \\ y = 1: u_{11} &= 0, \theta_{11} = 0 \end{aligned} \quad (40)$$

### 3.3 Finite difference method

Obtaining exact solution for the above fourth order differential equation is difficult, so substituting the following finite difference formulae

$$\frac{dv_{11}}{dy} = \frac{v_{11}(i+1) - v_{11}(i-1)}{2h}$$

$$\frac{d^2 v_{11}}{dy^2} = \frac{v_{11}(i+1) - 2v_{11}(i) + v_{11}(i-1)}{h^2}$$

$$\frac{d^3 v_{11}}{dy^3} = \frac{v_{11}(i+2) - 2v_{11}(i+1) + 2v_{11}(i-1) - v_{11}(i-2)}{2h^3}$$

$$\frac{d^4 v_{11}}{dy^4} = \frac{v_{11}(i+2) - 4v_{11}(i+1) + 6v_{11}(i) - 4v_{11}(i-1) + v_{11}(i-2)}{h^4}$$

inequation (34), the following system of equations are obtained

$$B_1 v_{11}(i+2) + B_2 v_{11}(i+1) + B_3 v_{11}(i) + B_4 v_{11}(i-1) + B_5 v_{11}(i-2) = 0 \quad (41)$$

with boundary conditions in finite difference form:

$$v_{11}[i] = 0, \text{ for } i = 0$$

$$v_{11}[i] = 0, \text{ for } i = 10$$

where

$$B_1 = 2 - \text{Re } h$$

$$B_2 = -8 + 2\text{Re } h - 2h^2 \left( M^2 + \frac{1}{K} + 2\pi^2 \right) + \text{Re } h^3 \pi^2$$

$$B_3 = 12 + 4h^2 \left( M^2 + \frac{1}{K} + 2\pi^2 \right) + 2h^4 \left( \pi^4 + \frac{\pi^2}{K} \right)$$

$$B_4 = -8 - 2\text{Re } h - 2h^2 \left( M^2 + \frac{1}{K} + 2\pi^2 \right) - \text{Re } h^3 \pi^2$$

$$B_5 = 2 + \text{Re } h$$

Similarly substitution of the following finite difference formulae

$$\frac{dg}{dy} = \frac{g(i+1) - g(i-1)}{2h}$$

$$\frac{d^2g}{dy^2} = \frac{g(i+1) - 2g(i) + g(i-1)}{h^2} \text{ where } g \text{ stands } u_{11} \text{ and } \theta_{11},$$

into equations (38) and (39), gives the following system of equations

$$B_1 u_{11}(i+1) - B_6 u_{11}(i) + B_5 u_{11}(i-1) = B(i) \tag{42}$$

$$D_1 \theta_{11}(i+1) - D_2 \theta_{11}(i) + D_3 \theta_{11}(i-1) = D(i) \tag{43}$$

with conditions in finite difference form :

$$u_{11}[i] = 0, \theta_{11}[i] = 1, \text{ for } i = 0$$

$$u_{11}[i] = 0, \theta_{11}[i] = 0, \text{ for } i = 10$$

where  $i$  stands plate divisions with step length  $h=0.1$  and  $y = i h$ ,

$$D_1 = 2 - R_e P_r h, D_2 = 4 + 2(\pi^2 - S)h^2$$

$$D_3 = 2 + R_e P_r h, B_6 = 4 + 2h^2 \left( M^2 + \frac{1}{K} + \pi^2 \right)$$

$$B(i) = R_e v_{11}(i) \left( \frac{m_1 e^{m_1 i h} - m_2 e^{m_2 i h}}{e^{m_1} - e^{m_2}} \right)$$

$$D(i) = \text{Re Pr } v_{11}(i) \left( \frac{a_2 e^{a_2 i h} - a_1 e^{a_1 i h}}{e^{a_2} - e^{a_1}} \right)$$

Equations (41), (42) and (43) have been solved using Gauss-seidel iteration method and to obtain the solution of this system a numerical code is executed using C-Program. In order to prove the convergence of finite difference scheme, computation is carried out for slightly changed value of  $h$  and the iterations on until a **tolerance**  $10^{-8}$  is attained. No significant change was observed in the values of temperature profile ( $\theta$ ), main and cross flow velocities  $w$  &  $\theta$  respectively. Thus, it is concluded that the finite difference scheme is convergent and stable.



#### 4 Nusselt-number:

From the temperature field the heat transfer coefficient in terms of Nusselt number  $Nu$  is given by

$$Nu = \frac{-d.q_w^*}{k(T_0 - T_1)} = \left( \frac{d\theta_0}{dy} + \varepsilon \frac{d\theta_{11}}{dy} \cos \pi z \right)_{y=0} \quad (46)$$

#### Nomenclature

$\rho$	Density of the fluid
$p^*$	Pressure
$K^*$	Permeability of the porous medium
$\nu$	Kinematic viscosity
$k$	Thermal conductivity
$B_0$	Magnetic field component along $y^*$ -axis,
$\sigma$	Electrical conductivity
$\mu$	Viscosity
$C_p$	Specific heat at constant pressure
$S$	Heat source parameter

#### 5 Results and Discussion

In order to explore the importance of the various physical parameters involved in this study, a parametric study of the physical parameters is conducted in the presence of heat source. During the course of numerical calculations, to be realistic, the values of Prandtl number (Pr) are chosen to be 0.71, 7.0 and 11.4 representing air, water at 20<sup>0</sup> C and water at 4<sup>0</sup> C respectively.

Figure (1) shows the temperature profile for various values of heat generation parameter (S). It is evident from the figure that temperature of the fluid increases with increasing values of heat source parameter S. Figure (2) depicts the effect of Prandtl number Pr on temperature field ( $\theta$ ) in the presence of heat source. It is observed that the presence of heavier Prandtl number fluid is found to decelerate the temperature at all the points in the flow field. This is due to the fact that a fluid with higher Prandtl number has relatively lower thermal conductivity. Figure (3) is drawn for various selected values of injection/suction parameter Re on temperature profile ( $\theta$ ) in the presence of heat source. A comparative study of the graph reveals that the temperature of the fluid increases in the presence of heat source parameter. This result qualitatively agrees with the physical fact that heat generation is to increase the rate of heat transport to the fluid there by increasing the temperature of the fluid. Further it is noted that temperature decreases with increasing values injection/suction parameter (Re).

The main flow velocity profile is shown graphically in figure (6) for various values of the magnetic parameter M. It is noted from figure that the increasing values of magnetic parameter is to reduce the velocity of the flow. This is due to the fact that the introduction

of magnetic field normal to the fluid flow has a tendency to give rise to a resistive-type force called the Lorentz force, which acts against the fluid flow and hence results in reducing the velocity profile due to this type of magnetic pull of Lorentz force.

Figure (7) depicts the main flow velocity profile for small and large values of permeability and for various smaller values of injection/suction parameter ( $Re$ ). It is observed from figure that an increase in  $Re$  leads to decrease in the velocity while an increase in permeability of the porous medium leads to increase in the velocity of the fluid flow. Also it is observed that the dotted line in the figure shows a Couette flow in ordinary medium as the value of  $Re$  is considered to be zero, it means that there is no injection and suction at lower and upper plates respectively. Figure (8) shows the effect of magnetic parameter  $M$  on cross flow velocity. It is observed from figure that for the increasing values magnetic parameter  $M$ , cross flow velocity is found to increase near the lower and upper half of the plates. But a reverse phenomenon is observed in the middle of the channel. This is due to the fact that there is an injection at the stationary plate and the constant suction at the plate in uniform motions, which are two exactly opposite processes.

Figures (4), (9) and (5) are plotted for Nusselt number versus various values of injection/suction parameter  $Re$  in the case of  $Pr=0.71$  and  $7.0$  respectively. It is observed that Nusselt number increases in the presence of heat source while it decreases with the increasing values of  $Re$ . Further, it is interesting to note that the effect of heat source on Nusselt number is more significant in the case of  $Pr=0.71$ , than in the case of  $Pr=7.0$ . The graphical results obtained for Nusselt number in the absence of heat source parameter, show a good agreement with previously published work [11]. Figure (10) shows that Nusselt number 'Nu' versus 'Re' for various values of  $Pr$  and  $K$ . It is observed that the results obtained in the absence of heat source and magnetic parameters are almost all similar to the results of K.D Singh [11]. The obtained results are in accordance with the physical realities which validate the correctness of our work presented here.

### **Conclusions**

Effect of heat source on Couette flow of a viscous incompressible electrically conducting fluid between two horizontal parallel porous flat plates is analyzed. From this study the following conclusions are drawn.

- (1) Temperature and Nusselt number increase in the presence of heat source. This is due to the fact that the effect of heat generation is to increase the rate of heat transport to the fluid.
- (2) The effect of heat source on Nusselt number is more significant in the case  $Pr=0.71$  than in the case  $Pr=7.0$
- (3) A growing magnetic parameter reduces the main flow velocity ( $u$ ) due to the magnetic pull of the Lorentz force. But it accelerates the cross flow velocity near the lower and upper half of the plates.
- (4) The results of the validation of this work in the absence of heat source and magnetic parameter agree significantly with the graphical results of K.D Singh [11].

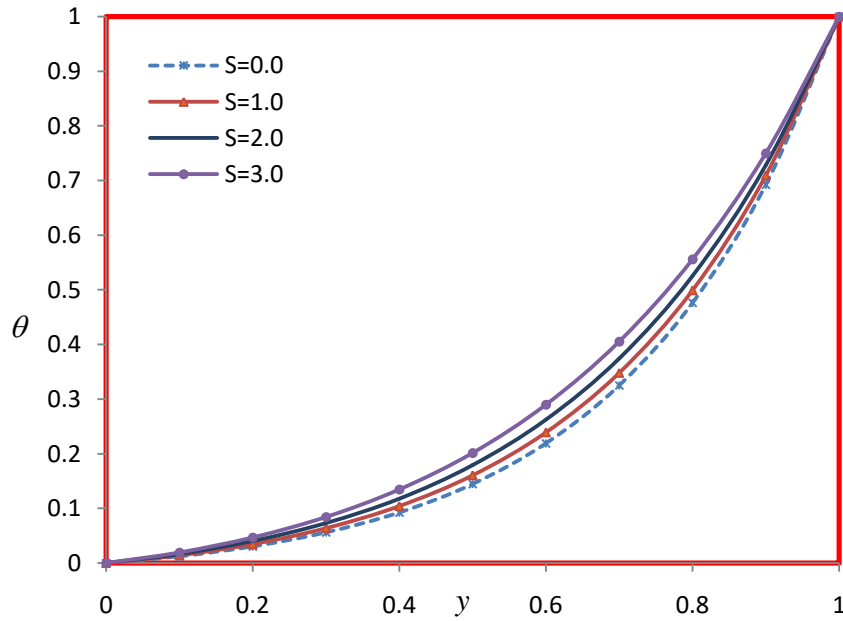


Fig1: Temperature profile for  $Re=5.0$ ,  $Pr=0.71$ ,  $M=1.0$ ,  $Z=0.5$ ,  $\epsilon=0.2$  and  $K=0.2$

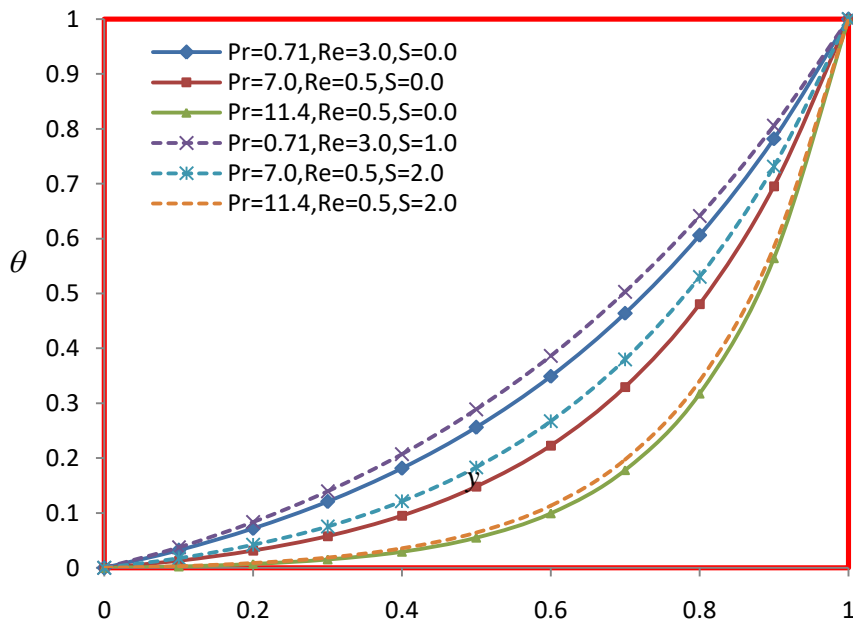


Fig2: Temperature profile for  $M=1.0$ ,  $Z=0.5$ ,  $\epsilon=0.2$  and  $K=0.2$

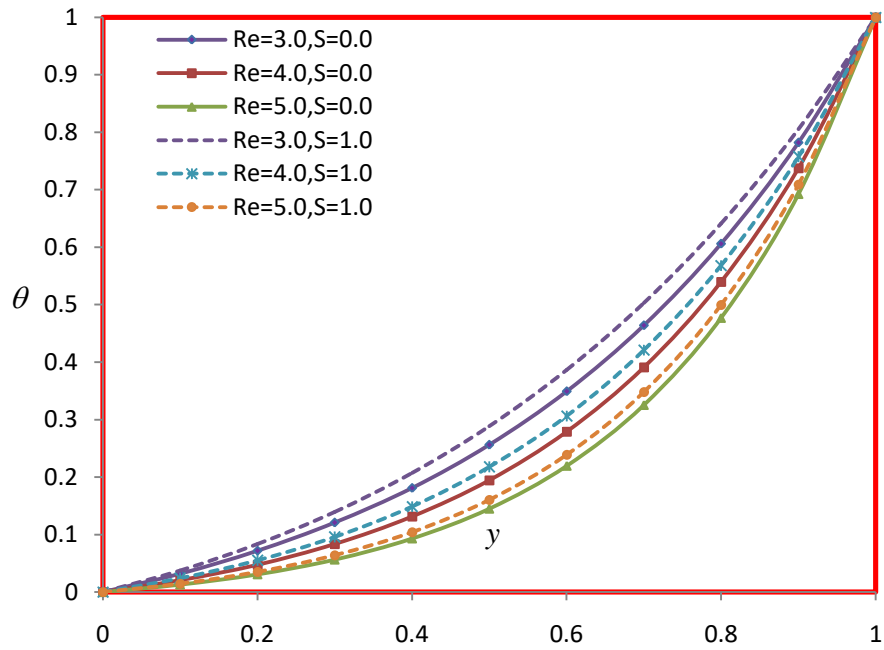


Fig3: Temperature profile for  $Pr=0.71, M=1.0, Z=0.5, \epsilon=0.2$  and  $K=0.2$

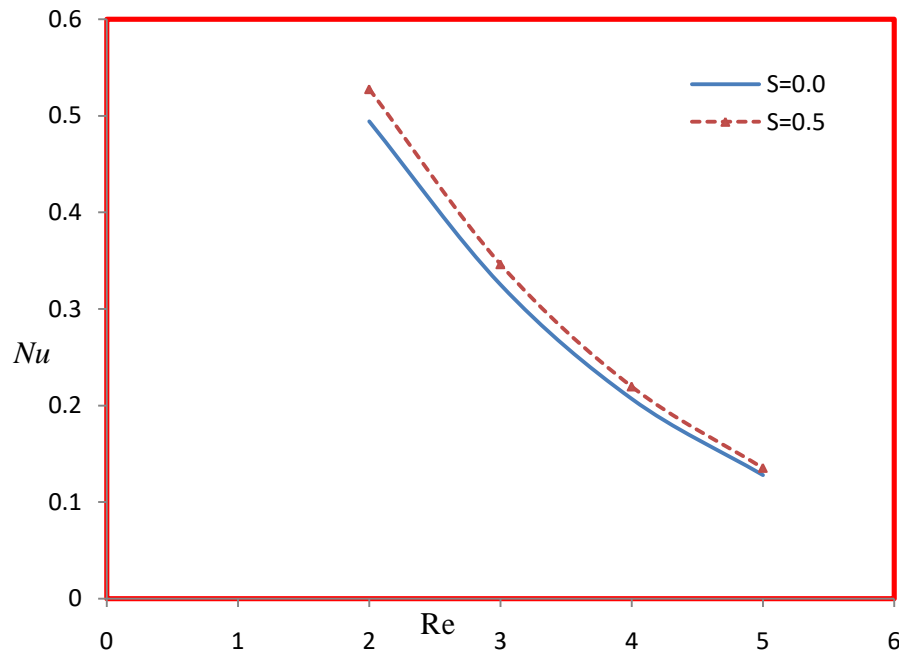


Fig4: Nusselt number for  $Pr=0.71, M=1.0, Z=0.5, \epsilon=0.2$  and  $K=0.2$

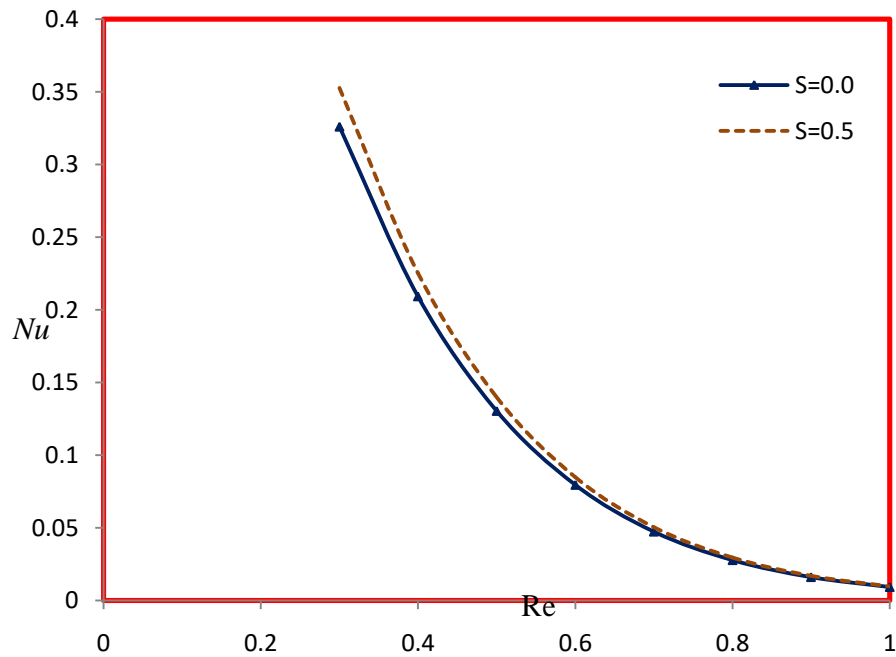


Fig5: Nusselt number for Pr=7.0, M=1.0, Z=0.5, ε=0.2 and K=0.2

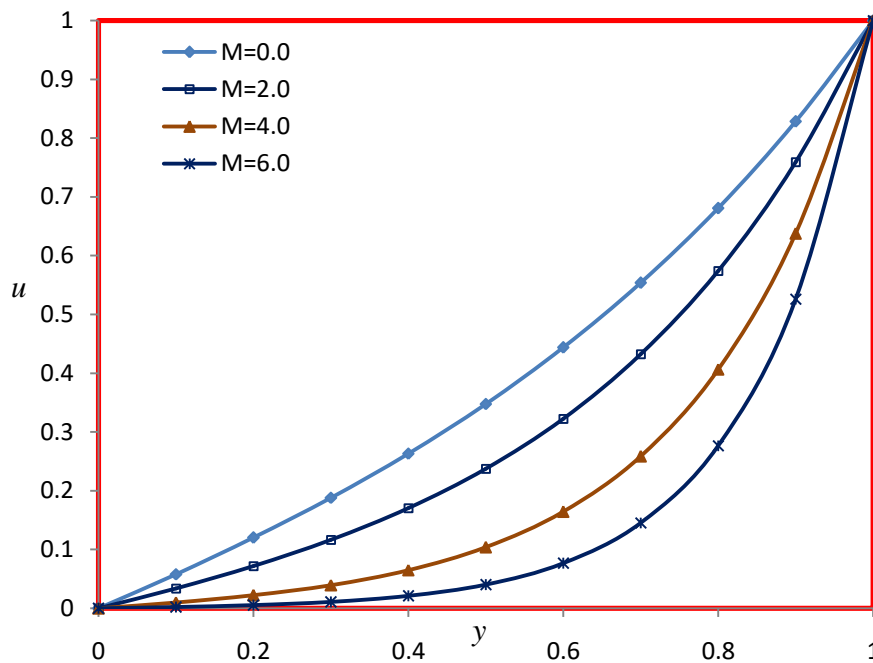


Fig 6: Main flow velocity profile u for Z=0.0, ε=0.2 and K=0.2

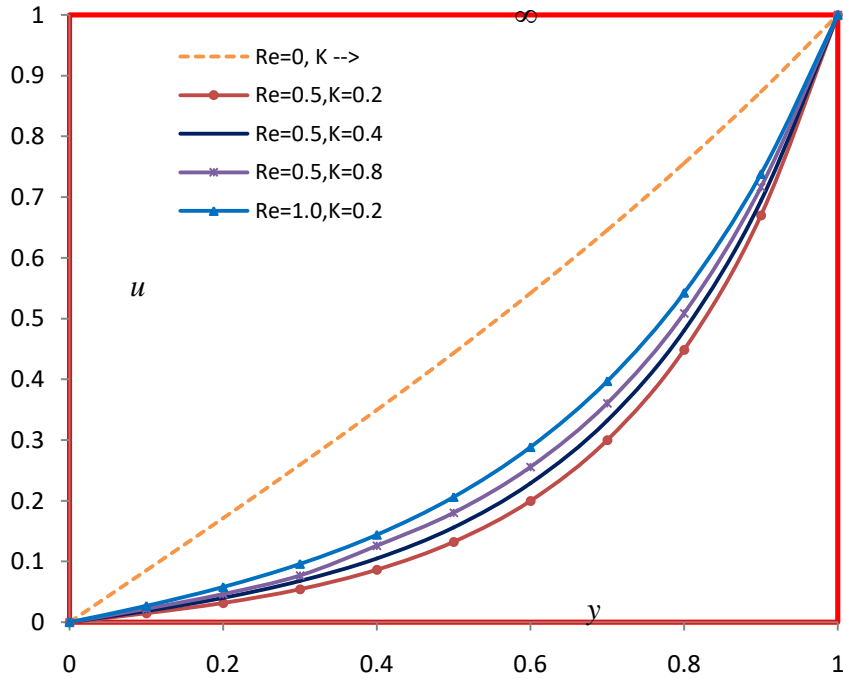


Fig 7: Main flow velocity profile  $u$  for  $Z=0.0$ ,  $\epsilon=0.2$  and  $K=0.2$

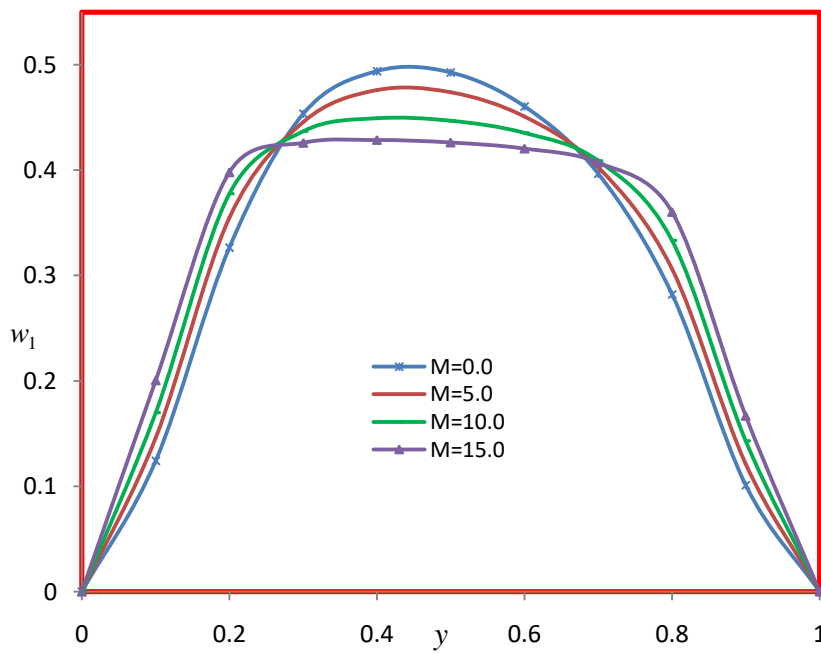


Fig 8: Effect of magnetic parameter  $M$  on cross flow velocity ( $Z=0.0$ ,  $\epsilon=0.2$ ,  $K=0.2$ ,  $Re=0.5$ )

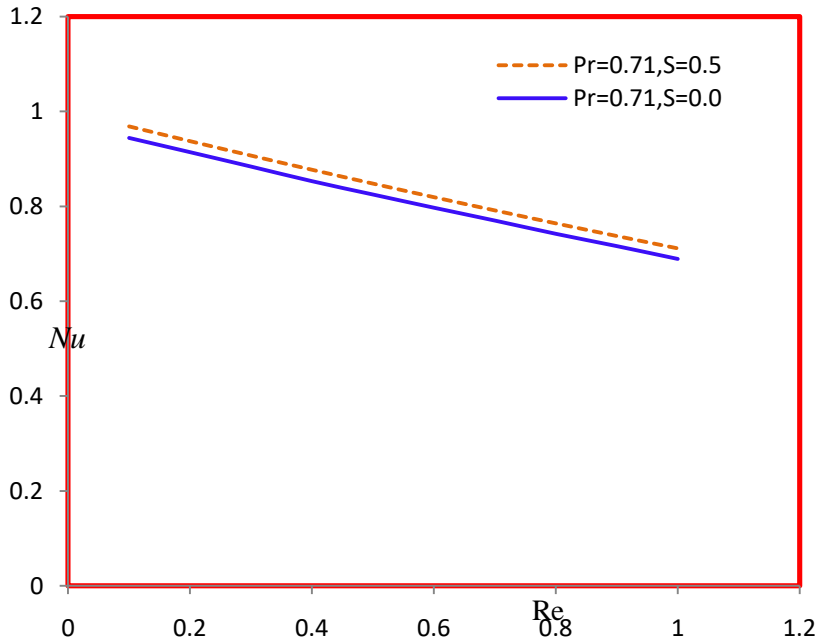


Fig 9: Nusselt number Nu versus Re for M=1.0, K=0.2 and Z=0.5, ε=0.2

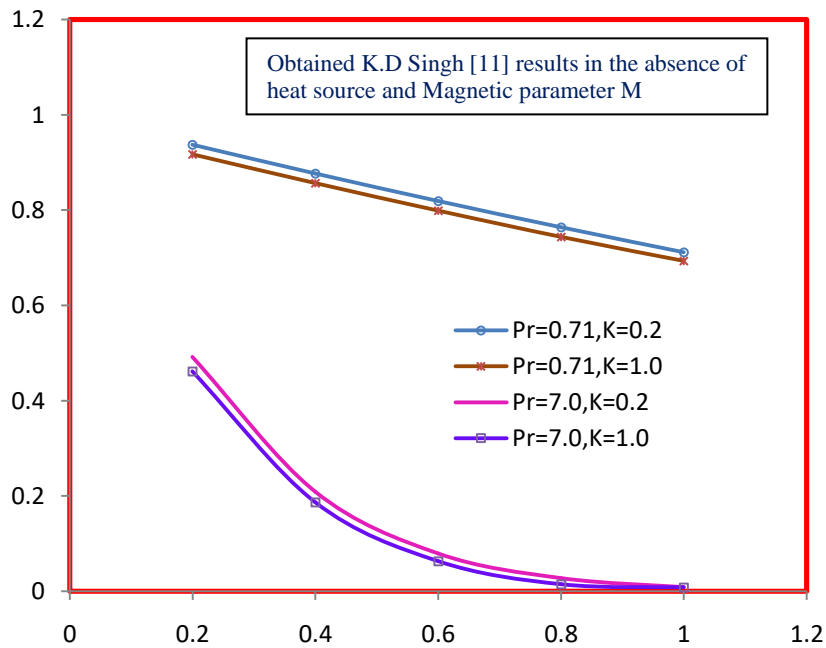


Fig 10: Nusselt number Nu versus 'Re' for Z=0.5, ε=0.2

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